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| 10/541,432 | 07/05/2005 | Ermanno Filippi | 9526-57 | 6387 |
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| P.O. BOX 3188 | } | BHAT, NINA NMN | | |
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Please find below and/or attached an Office communication concerning this application or proceeding.

The time period for reply, if any, is set in the attached communication.

| | | Application | ı No. | Applicant(s) | | |
|---|---|---|--|--|-------------|--|
| Office Action Summary | | 10/541,432 | 2 | FILIPPI ET AL. | | |
| | | Examiner | | Art Unit | | |
| | | N. Bhat | | 1797 | | |
| The MAILING D. Period for Reply | ATE of this communication | appears on the | cover sheet with the c | correspondence ad | ddress | |
| A SHORTENED STAT WHICHEVER IS LONG - Extensions of time may be av after SIX (6) MONTHS from t - If NO period for reply is speci - Failure to reply within the set | UTORY PERIOD FOR REIGHT. SER, FROM THE MAILING ailable under the provisions of 37 CFR ne mailing date of this communication. fied above, the maximum statutory per or extended period for reply will, by state ce later than three months after the mate. See 37 CFR 1.704(b). | EDATE OF THI R 1.136(a). In no ever riod will apply and will atute, cause the applic | S COMMUNICATION It, however, may a reply be tine expire SIX (6) MONTHS from tation to become ABANDONE | N. nely filed the mailing date of this of D (35 U.S.C. § 133). | · | |
| Status | | | | | | |
| 2a)⊠ This action is FII 3)□ Since this applic | ommunication(s) filed on <u>04</u> NAL. 2b) To ation is in condition for allowance with the practice under | This action is now wance except f | n-final. or formal matters, pro | | e merits is | |
| Disposition of Claims | | | | | | |
| 4a) Of the above 5) ☐ Claim(s) i 6) ☑ Claim(s) <u>1-4</u> is/a 7) ☐ Claim(s) i 8) ☐ Claim(s) a Application Papers 9) ☐ The specification | re rejected. s/are objected to. are subject to restriction and is objected to by the Exam | drawn from con | quirement. | | | |
| Applicant may not Replacement draw | led on <u>05 July 2005</u> is/are: request that any objection to the ving sheet(s) including the contraction is objected to by the | the drawing(s) be rection is require | held in abeyance. Seed if the drawing(s) is ob | e 37 CFR 1.85(a). jected to. See 37 C | ` ' | |
| Priority under 35 U.S.C. { | § 119 | | | | | |
| 12) Acknowledgment is made of a claim for foreign priority under 35 U.S.C. § 119(a)-(d) or (f). a) All b) Some * c) None of: 1. Certified copies of the priority documents have been received. 2. Certified copies of the priority documents have been received in Application No 3. Copies of the certified copies of the priority documents have been received in this National Stage application from the International Bureau (PCT Rule 17.2(a)). * See the attached detailed Office action for a list of the certified copies not received. | | | | | | |
| Attachment(s) 1) Notice of References Cited 2) Notice of Draftsperson's P 3) Information Disclosure Sta | atent Drawing Review (PTO-948) | | 4) Interview Summary Paper No(s)/Mail Da 5) Notice of Informal F 6) Other: | ate | | |

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DETAILED ACTION

1. Applicant's arguments and remarks of September 4, 2008 have been fully and carefully considered but have not been found persuasive, applicant has not amended any of the claims, the claims remain as originally filed on July 5, 2005.

2. Claims 1-4 remain rejected under 35 U.S.C. 103(a) as being unpatentable over Agarwal, EP 0094208 in combination with Filippi et al., EP 1153653.

Agarwal teach the invention substantially as claimed. Specifically Agarwal teach a temperature controls system which controls the temperate of a reactor by controlling in flow lines and using parameters of known quantities for specific heat of the feed, the effluent and heat of vaporization and reaction to calculate a coolant flow rate set point. The system and method as taught by Agarwal includes a reactor having a feed line for reactant and an effluent line for the product, a feed flow transmitter connected to the feed line for measuring the reactant flow; a effluent flow transmitter which is connected to the effluent line for measuring the flow of product from the reactor; a feed temperature transmitter connected to the feed line for sensing the reactant temperature, and effluent temperature transmitter for measuring the product temperature. A reactor temperature transmitter which measures the temperature of the reactor, a concentration transmitter connected to the effluent line for measuring the concentration of product in the effluent line, a coolant flow line to the reactor for supplying coolant to the reactor at a coolant flow rate, a coolant flow control means and circuit means that connects to all of the transmitters and to the coolant flow control means for controlling the flow of coolant to the reactor according to the coolant flow signal which is connected to receive quantities proportional to the heat of reaction for at least one reaction in the reactor, specific heats of the reactant and product and the heat of vaporization of the coolant.[Note the abstract, Page 3, line 1-30 and The heat and temperature and flow control algorithms as taught in Agarwal is fully capable of setting

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the speed of the heat exchange fluid inside the respective heat exchange within predetermined value so that the heat exchange coefficient inside the heat exchanger is less than the heat exchange coefficient in the catalytic bed.

However, Agarwal does not teach that the two heat exchanger is disposed within catalytic bed nor the specific relationship that the heat exchange coefficient inside the heat exchangers is equal to or less than 2/3 of the heat exchange coefficient inside the catalytic bed.

Filippi et al. '653 teach a fixed bed reactor for carrying out exothermic or endothermic reactions which includes a heat exchanger (9) embedded in a catalytic layer (10).[Note Paragraph[0023] Filippi et al. teach the construction arrangement of the heat exchangers within the reactor provides an isothermal reactor having high heat exchange degree that allows an optimum control of the temperature to the advantage of higher conversion yield and improved or lowered energy consumption. Filippi et al. teach that the high heat exchange efficiency inside the reactor allows recovering or supplying heat with smaller temperature differences between there reactant fluid and heating or cooling fluid. The construction and arranged provides a smaller gradient of temperature inside the catalytic layer between two adjacent heat exchange plates thereby achieving a greater uniformity of temperature inside the catalytic layer.[Note [0030]]. The reactor as described by Filippi et al. is fully capable of carrying out chemical reactions in pseudo-isothermal conditions.

It would have been obvious from the combined teachings of Agarwal and Filippi et al. to provide a temperature control system which is capable of adjusting the temperature inside a reaction zone of a catalytic reactor, includes probes/sensors for measuring the temperature between zones between the heat exchanger surface and catalyst and being capable of controlling the flow rate of the fluids inside the heat exchanger thereby modifying the heat exchange coefficient. It is maintained that the control system and algorithms described by

Agarwal is capable of controlling the reaction temperature in a catalytic bed of a reactor in which the exchange is carried out so as to allow the transfer of the larges possible amount of heat between operating fluid and catalytic bed and maximizing the heat exchange coefficient inside the exchangers. Agarwal specifically teach sensing input and output streams, flow streams within the reactor and within the heat exchanger and manipulating the heat exchange fluid streams which provides conditions within the reactor to maximize and optimize the yield of reaction and reaction conditions. To use the control system in a reactor taught by Filippi wherein the reactor is specifically designed to operate under isothermal conditions which includes a fixed bed reactor, the heat exchangers disposed within the reactor and wherein the conditions of the reactor are controlled so that chemical reaction takes place in a pseudo isothermal conditions wherein the heat exchanger is crossed by a respective operating fluid immersed in the catalytic bed renders applicant's invention as a whole obvious and a permissible substitution to one having ordinary skill in the art at the time the invention was made.

Applicant has argued that the temerpature control of Agarwal is totally different in nature than claimed in claim 1 wherein the reaction temperature is controlled by means of heat exchanger immersed in a catalytic bed. Applicant is arguing each reference singularly not what the combination of what the references teach. In response to applicant's arguments against the references individually, one cannot show nonobviousness by attacking references individually where the rejections are based on combinations of references. See *In re Keller*, 642 F.2d 413, 208 USPQ 871 (CCPA 1981); *In re Merck & Co.*, 800 F.2d 1091, 231 USPQ 375 (Fed. Cir. 1986). Specifically, the reactor which includes the two heat exchangers disposed within the catalytic bed is taught by Filippi et al. Filippi et al. further teach operating the reactor under isothermal conditions which would require the heat transfer coefficient to be adjust because the

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temperatures within the reactor are being controlled. Agarwal teaches the concept of adjusting the temperature inside a reaction zone and provides the teaching of providing a probe (probes) for continuously measuring the temperature difference between different zones within the reactor and then correlating and this data and adjusting accordingly.

Because the heat transfer coefficient is defined by

 $h = \Delta Q/A \cdot \Delta T \cdot \Delta t$

where

 ΔQ = heat input or heat lost, J

 $h = \text{heat transfer coefficient}, W/(m^2K)$

 $A = \text{heat transfer surface area, m}^2$

 ΔT = difference in temperature between the solid surface and surrounding fluid area, K

 Δt = time period, s

From the above equation, the heat transfer coefficient is the <u>proportionality</u> coefficient between the heat <u>flux</u>, $Q/(A\Delta t)$, and the thermodynamic driving force for the flow of heat (i.e., the temperature difference, ΔT).

The reactors of Filippi et al. is constructed and arranged such that the reactor operates in isothermal conditions which means that the reactor will operate in which the temperature of the system remains constant. The heat transfer into or out of the system typically must happen at such a slow rate that the thermal equilibrium is maintained. In such cases, the heat transfer coefficient would be adjusted such that equilibrium or heat transfer is maintained in order to keep the temperature of the system constant. It is therefore maintained that as claimed applicant's method and apparatus is rendered obvious to one having ordinary skill in the art at the time the invention was made.

3. **THIS ACTION IS MADE FINAL**. Applicant is reminded of the extension of time policy as set forth in 37 CFR 1.136(a).

A shortened statutory period for reply to this final action is set to expire THREE MONTHS from the mailing date of this action. In the event a first reply is filed within TWO

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MONTHS of the mailing date of this final action and the advisory action is not mailed until after the end of the THREE-MONTH shortened statutory period, then the shortened statutory period will expire on the date the advisory action is mailed, and any extension fee pursuant to 37 CFR 1.136(a) will be calculated from the mailing date of the advisory action. In no event, however, will the statutory period for reply expire later than SIX MONTHS from the mailing date of this final action.

4. Any inquiry concerning this communication or earlier communications from the examiner should be directed to N. Bhat whose telephone number is 571-272-1397. The examiner can normally be reached on Monday-Friday, 9:30AM-6:00PM.

If attempts to reach the examiner by telephone are unsuccessful, the examiner's supervisor, Glenn Caldarola can be reached on 571-272-1444. The fax phone number for the organization where this application or proceeding is assigned is 571-273-8300.

Information regarding the status of an application may be obtained from the Patent Application Information Retrieval (PAIR) system. Status information for published applications may be obtained from either Private PAIR or Public PAIR. Status information for unpublished applications is available through Private PAIR only. For more information about the PAIR system, see http://pair-direct.uspto.gov. Should you have questions on access to the Private PAIR system, contact the Electronic Business Center (EBC) at 866-217-9197 (toll-free). If you would like assistance from a USPTO Customer Service Representative or access to the automated information system, call 800-786-9199 (IN USA OR CANADA) or 571-272-1000.

/N. Bhat/ Primary Examiner, Art Unit 1797